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| Name: Enrolment No: |  |
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UNIVERSITY OF PETROLEUM AND ENERGY STUDIES
End Semester Examination, May 2022

Course: Chemical Reaction Engineering-II
Program: B.Tech. CE+RP
Course Code: CHCE3031

Semester: VI
Time : 03 hrs.
Max. Marks: 100

Instructions: (i) This question paper have total 03 Sections. All questions are compulsory.
(ii) Attempt all the sub-parts of a question together.

SECTION A
(5Qx4M=20Marks)

| S. No. | | Marks | CO |
|--------|---|-----------|------------|
| Q 1 | Define residence time distribution and write the relation between C and E. | 04 | CO1 |
| Q 2 | Discuss the significance of tank in series model. | 04 | CO2 |
| Q 3 | Does a catalyst alter equilibrium conversion of a chemical reaction? Explain. | 04 | CO5 |
| Q 4 | What is sol gel method of preparation of catalyst? | 04 | CO3 |
| Q 5 | What is the importance of pores in a catalyst particle? Differentiate micro and macro pore. | 04 | CO4 |

SECTION B
(4Qx10M= 40 Marks)

| Q 6 | Develop Langmuir Hinshelwood model for the following reaction when adsorption of A is rate limiting step $A + B \rightleftharpoons R + S$ | 10 | CO3 | | | | | | | | | | | | | | |
|-------------------|---|-----------|------------|-------|-------|--------------|---|--------------|-------------------|-------|-------|-------|-------|-------|-------|-----------|------------|
| Q 7 | Derive an expression for first order solid catalyzed reaction considering pore diffusion. | 10 | CO3 | | | | | | | | | | | | | | |
| Q 8 | The following data on an irreversible reaction are obtained with decaying catalyst in a batch reactor (batch-solids, batch-fluid) What can you say about the kinetics <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="width: 10%;">t, hr</th> <th style="width: 10%;">0</th> <th style="width: 10%;">0.25</th> <th style="width: 10%;">0.5</th> <th style="width: 10%;">1</th> <th style="width: 10%;">2</th> <th style="width: 10%;">(∞)</th> </tr> </thead> <tbody> <tr> <td>C_A, mol/liter</td> <td>1.000</td> <td>0.901</td> <td>0.830</td> <td>0.766</td> <td>0.711</td> <td>0.684</td> </tr> </tbody> </table> | t, hr | 0 | 0.25 | 0.5 | 1 | 2 | (∞) | C_A , mol/liter | 1.000 | 0.901 | 0.830 | 0.766 | 0.711 | 0.684 | 10 | CO5 |
| t, hr | 0 | 0.25 | 0.5 | 1 | 2 | (∞) | | | | | | | | | | | |
| C_A , mol/liter | 1.000 | 0.901 | 0.830 | 0.766 | 0.711 | 0.684 | | | | | | | | | | | |

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| Q 9 | Discuss and derive the dispersion model to describe the non-ideal behavior in tubular flow reactor. | 10 | CO2 |
| SECTION-C (2Qx20M=40 Marks) | | | |
| Q 10 | The decomposition of cumene is carried out over the platinum catalyst to form benzene and propylene. Draw a conceptual model depicting the sequences of the steps in this reaction and derive the rate law if surface reaction is the rate limiting. | 20 | CO4 |
| Q 11 | <p>(a) Sketch and explain the RTD curve for ideal Plug flow and ideal batch reactor.</p> <p>(b) We want to perform in a tank reactor the liquid phase reaction $2A \rightarrow B$ It has been determined that the rate equation is:</p> $r = \frac{0.5 C_A}{1+0.5 C_A} \quad (r \text{ in mol. L}^{-1} \cdot \text{h}^{-1} \text{ and } C_A \text{ in mol/L})$ <p>In order to characterize the reactor, a pulse tracer test was performed, after which it was obtained that the tracer concentration measured versus time can be fitted to the following equation: $C(t) = 2 \exp(-2t) \quad (C \text{ in mg/L and } t \text{ in h})$</p> <p>a) Calculate $E(t)$ and the average time in the reactor t_m. b) Calculate $F(t)$. Which fraction of the effluent will remain in the reactor after the first hour after injection of the tracer?</p> | 10+10 | CO1 |