

Name:	
Enrolment No:	

UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

End Semester Examination, May 2021

Programme Name: B. Tech in Applied Petroleum Engineering, Spl. Gas	Semester : IV
Course Name : Mass Transfer	Time : 03 hrs.
Course Code : CHCE 2017	Max. Marks : 100
Nos. of page(s) : 2	

Instructions: The exam will be OPEN BOOK and OPEN NOTES exam. The students are allowed any textbooks, photo-copied and hand-written notes. The students will need graph papers

SECTION A [30]

S. No.		Marks	CO														
Q1.	a. What is the significance of “Chemical Potential” in mass transfer operations? Answer in detail.	[5]	CO1														
	b. Starting from $N_A = N \cdot X_A + J_A$, show that $j_A = \rho_A (v_A - v)$ Here, N , N_A and J_A are the molar fluxes in $\text{kmol/m}^2\cdot\text{sec}$ and j_A and j_B are mass fluxes in $\text{kg/m}^2\cdot\text{sec}$. ρ_A is the density and v_A , v are the velocities.	[10]	CO1														
Q2.	<p>A solution containing 60% A and 40% C is fed to a <u>co-current</u> extractor at 120 kmol/hr. Solvent B is added to the process at 200 kmol/hr.</p> <p>a. Calculate the amount of C removed for the above condition.</p> <p>b. Calculate the amount of C removed if the process is converted to a <u>2 staged cross current process</u> with 100 kmol/hr of B added to each stage. Write what do you infer from both the results.</p> <p>The equilibrium data is as below</p> <table border="1" style="margin-left: auto; margin-right: auto; border-collapse: collapse;"> <tr> <td style="padding: 2px;">X (kmol of C per kmol of A)</td> <td style="padding: 2px;">0.05</td> <td style="padding: 2px;">0.2</td> <td style="padding: 2px;">0.3</td> <td style="padding: 2px;">0.45</td> <td style="padding: 2px;">0.5</td> <td style="padding: 2px;">0.54</td> </tr> <tr> <td style="padding: 2px;">Y (kmol of C per kmol of B)</td> <td style="padding: 2px;">0.25</td> <td style="padding: 2px;">0.4</td> <td style="padding: 2px;">0.5</td> <td style="padding: 2px;">0.65</td> <td style="padding: 2px;">0.7</td> <td style="padding: 2px;">0.74</td> </tr> </table> <p><i>Instruction: Please plot the graph using the same graph paper</i></p>	X (kmol of C per kmol of A)	0.05	0.2	0.3	0.45	0.5	0.54	Y (kmol of C per kmol of B)	0.25	0.4	0.5	0.65	0.7	0.74	[15]	CO2
X (kmol of C per kmol of A)	0.05	0.2	0.3	0.45	0.5	0.54											
Y (kmol of C per kmol of B)	0.25	0.4	0.5	0.65	0.7	0.74											

SECTION B [30]

Q3.	<p>a. Explain how heat and mass transfer are simultaneously affecting the process of drying and humidification.</p> <p>b. If a solid is partially soaked in water, how will the process of drying occur? Please explain in terms of movement of water molecules.</p>	[15]	CO3
Q4.	<p>Crude with 0.8% H_2S fed at 1500 Kmol/hr is treated in a packed column with ethanolamine solution containing 0.02% H_2S. The optimum liquid rate is 2.5 times the minimum liquid flowrate. If the packed column of diameter 2 m is filled in random with 2.5 in glass saddle packings, <u>calculate the height of the packing</u> required to separate 98% of H_2S from the crude. The mass transfer coefficient for the process $K_{Ga} = 1450 \text{ Kmol/hr. m}^3$ and equilibrium condition follows the equation $y^* = 1.5x$. The minimum liquid flowrate for the process is 1090 Kmol/hr.</p>	[15]	CO4

SECTION-C [40]

- Q5. 55% Butane and 45% Hexane mixture is separated in a distillation column operated at 1 atm pressure and 45°C. The Distillate is removed at 450 kmol/hr and has composition of 90% and the bottom has 92%. The optimum reflux is 2 times the minimum reflux. The feed condition is an equal mixture of vapor and liquid.
- Calculate the Real number of trays required for the process if the efficiency is 68%.
 - Calculate the optimum feed tray location
 - Feed flowrate needed for the process.
 - What should be done to increase the purity of the product?

The equilibrium data is as below

y*	0.21	0.37	0.51	0.64	0.72	0.79	0.86	0.91	0.96	0.98
x	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	0.95

The x, y data are in mole fraction*

[40]

CO4