

<b>Name:</b>	
<b>Enrolment No:</b>	

**UNIVERSITY OF PETROLEUM AND ENERGY STUDIES**  
**End Semester Examination, December 2018**

**Course: PRINCIPLES OF RESERVOIR ENGINEERING**

**Semester: VII**

**Programme: BTECH GSE**

**Time: 03 hrs.**

**Max. Marks: 100**

**Instructions: All questions are compulsory. There is no overall choice. However, internal choice has been provided. You have to attempt only one of the alternatives in all such questions.**

**SECTION A**

S. No.		Marks	CO												
1	<p>Given the following gas:</p> <table border="1" style="margin-left: 20px;"> <thead> <tr> <th>Component</th> <th>Weight fraction</th> </tr> </thead> <tbody> <tr> <td>C1</td> <td>0.65</td> </tr> <tr> <td>C2</td> <td>0.15</td> </tr> <tr> <td>C3</td> <td>0.10</td> </tr> <tr> <td>n-C4</td> <td>0.06</td> </tr> <tr> <td>n-C5</td> <td>0.04</td> </tr> </tbody> </table> <p>Calculate:</p> <ol style="list-style-type: none"> <li>Mole fraction of the gas</li> <li>Apparent molecular weight</li> <li>Specific gravity</li> <li>Specific volume at 300 psia and 120°F by assuming an ideal gas behaviour.</li> </ol>	Component	Weight fraction	C1	0.65	C2	0.15	C3	0.10	n-C4	0.06	n-C5	0.04	<b>4</b>	<b>CO1</b>
Component	Weight fraction														
C1	0.65														
C2	0.15														
C3	0.10														
n-C4	0.06														
n-C5	0.04														
2	A typical pressure-temperature phase diagram of an oil reservoir is characterised by quality lines that are closely spaced near the dew point curve. Define the properties of reservoir along with the liquid shrinkage curve.	<b>4</b>	<b>CO3</b>												
3	Diagrammatically represent the process of flash and differential liberation tests.	<b>4</b>	<b>CO3</b>												
4	Under which flowing condition the following equation is validated $dp/dr = 0$ at the boundary condition. Justify the answer.	<b>4</b>	<b>CO2</b>												
5	“When a wetting and a non wetting phase flow together in a reservoir rock, each phase follows separate and distinct paths.” Justify how the presence of one phase effects the fluid flow in porous and permeable media with the help of a graph.	<b>4</b>	<b>CO2</b>												
<b>SECTION B</b>															
6	Calculate the average permeability of a formation that consists of four beds in series, assuming:	<b>10</b>	<b>CO2</b>												

	<p>a. Linear system b. Radial system with <math>r_w=0.3</math>ft and <math>r_e=1,450</math> ft.</p> <table border="1" data-bbox="201 338 911 527"> <thead> <tr> <th>Bed</th> <th>Length of bed (ft)</th> <th>Permeability (mD)</th> </tr> </thead> <tbody> <tr> <td>1</td> <td>400</td> <td>70</td> </tr> <tr> <td>2</td> <td>250</td> <td>400</td> </tr> <tr> <td>3</td> <td>300</td> <td>100</td> </tr> <tr> <td>4</td> <td>500</td> <td>60</td> </tr> </tbody> </table>	Bed	Length of bed (ft)	Permeability (mD)	1	400	70	2	250	400	3	300	100	4	500	60							
Bed	Length of bed (ft)	Permeability (mD)																					
1	400	70																					
2	250	400																					
3	300	100																					
4	500	60																					
7	<p>Define the following terms</p> <ol style="list-style-type: none"> <li>i. OFVF</li> <li>ii. Gas solubility</li> <li>iii. Effective porosity</li> <li>iv. Surface tension interfacial tension</li> <li>v. Cricondenbar temperature</li> <li>vi. Connate water saturation</li> <li>vii. Wettability</li> <li>viii. Free water level</li> <li>ix. Bubble point pressure</li> <li>x. Sub capillary pores</li> </ol>	<b>10</b>	<b>CO4</b>																				
8	<p>An oil well in the Nameless Field is producing at a stabilized rate of 600 STB/day at a stabilized bottom-hole flowing pressure of 1800 psi. Analysis of the pressure buildup test data indicates that the pay zone is characterized by a permeability of 120 md and a uniform thickness of 25ft. The well drains an area of approximately 40 acres. The following additional data is available:  <math>r_w = 0.25</math> ft <math>A = 40</math> acres  <math>B_o = 1.25</math> bbl/STB <math>\mu_o = 2.5</math> cp          Calculate the pressure profile (distribution) and list the pressure drop across 1 ft intervals from <math>r_w</math> to 1.25 ft, 4 to 5 ft, 19 to 20 ft, 99 to 100 ft, and 744 to 745 ft.</p> <p style="text-align: center;">OR</p> <p>Describe the basic assumptions behind Decline Curve Analysis. Explain the types of rate decline behavior with appropriate relationship curves.</p>	<b>10</b>	<b>CO4</b>																				
9	<p>During a PVT experiment a crude oil sample was placed in a variable volume cell and its initial bubble point pressure was determined. The pressure in the cell was then decreased in 3 steps and the volume of liquid and gases were recorded. After recording the value at each pressure the gas was purged out of the cell but all of the liquid retained. The temperature was kept constant at 15°C. The following data were recorded:</p> <table border="1" data-bbox="201 1667 1289 1894"> <thead> <tr> <th>Pressure (kpa)</th> <th>Volume of liquid (ml)</th> <th>Volume of gas released(ml)</th> <th>z-factor</th> </tr> </thead> <tbody> <tr> <td>30000</td> <td>189.75</td> <td>0</td> <td></td> </tr> <tr> <td>20000</td> <td>170.35</td> <td>24.97</td> <td>0.886</td> </tr> <tr> <td>10000</td> <td>159.85</td> <td>35.35</td> <td>0.932</td> </tr> <tr> <td>101.325</td> <td>147.83</td> <td>3981.35</td> <td>1</td> </tr> </tbody> </table>	Pressure (kpa)	Volume of liquid (ml)	Volume of gas released(ml)	z-factor	30000	189.75	0		20000	170.35	24.97	0.886	10000	159.85	35.35	0.932	101.325	147.83	3981.35	1	<b>10</b>	<b>C03</b>
Pressure (kpa)	Volume of liquid (ml)	Volume of gas released(ml)	z-factor																				
30000	189.75	0																					
20000	170.35	24.97	0.886																				
10000	159.85	35.35	0.932																				
101.325	147.83	3981.35	1																				

- Calculate OFVF at 30000kpa, 20000kpa and 10000kpa.
- Calculate solution GOR at 30000kpa, 20000kpa and 10000kpa.
- Calculate TFVF at 20000 kpa.

**SECTION-C**

10 Treating the reservoir pore as an idealized container derive the volumetric balance expression which occurs naturally during the productive life of a reservoir. Determine the relative magnitude of each of the driving mechanisms and its contribution to the production in a combination drive mechanism.

OR

A combination-drive reservoir contains 10 MMSTB of oil initially in place. The ratio of the original gas-cap volume to the original oil volume, i.e.,  $m$ , is estimated as 0.25. The initial reservoir pressure is 3000 psia at 150°F. The reservoir produced 1 MMSTB of oil, 1100 MMscf of 0.8 specific gravity gas, and 50,000 STB of water by the time the reservoir pressure dropped to 2800 psi. The following PVT is available:

	3000 psi	2800 psi
Bo, bbl/STB	1.58	1.48
Rs, scf/STB	1040	850
Bg, bbl/scf	0.0008	0.00092
Bt, bbl/STB	1.58	1.655
Bw, bbl/STB	1	1

The following data are also available:

$$S_{wi} = 0.20 \quad c_w = 1.5 \times 10^{-6} \text{ psi}^{-1} \quad c_g = 1 \times 10^{-6} \text{ psi}^{-1}$$

Calculate:

- Cumulative water influx
- Net water influx
- Primary driving indexes at 2800 psi

**20**

**CO5**

11 The following production data are available from a dry gas field:

Qt (MMscf/day)	Gp (MMscf)
320	16,000
336	32000
304	48000
309	96000
272	160000
248	240000
208	304000
197	352000
184	368000
176	384000
184	400000

Estimate

- The future cumulative gas production when the gas flow rate reaches

**20**

**CO6**

	80 MMscf/day (b) <i>Extra</i> time to reach 80 MMscf/day		
--	---	--	--